

Appendix

For first order plug flow reactor, the following kinetic equation will hold:

$$\text{WHSV}_{\text{MeOH}} = KC_{\text{MeOH}}M_{\text{MeOH}} / -\ln(1-X_{\text{MeOH}}) \text{---(1)}$$

Where,

K=rate constant, function of temperature

C_{MeOH} =MeOH concentration at reactor inlet (mol/ml)

M_{MeOH} =Methanol molecular weight

$\text{WHSV}_{\text{MeOH}}$ =weight hourly space velocity of methanol

X_{MeOH} =conversion of methanol

It is noted from equation (1) when temperature is not changed, $KC_{\text{MeOH}}M_{\text{MeOH}}$ remains constant. MeOH conversion X_{MeOH} should decrease with increase in $\text{WHSV}_{\text{MeOH}}$. Using this kinetic equation, by entering $\text{WHSV}_{\text{MeOH}}$ at 99.9% (13.4), we obtained $\text{WHSV}_{\text{MeOH}}$ at 57% conversion=109.7 h^{-1} , which is equivalent to $\text{LHSV}=249.6 \text{ h}^{-1}$ (S/C=1.78)

S/C=	1.78	w/w=	1.00125
LHSV=	30.5	Density=	0.88
Total WHSV=	26.84	g/cc.h	
WHSV MeOH=	13.41162	g/cc.h	
WHSV H2O	13.42838	g/cc.h	

Conversion at LHSV=30.5h ⁻¹	0.999	
Conversion at 57%	0.57	
Calculated WHSV MeOH at 57%	109.7719	g/cc.h
WHSV H2Oat 57%	109.9091	g/cc.h
Total LHSV	249.6374	h ⁻¹